Analyzing & Testing



NETZSCH Kinetics Neo Major Release 3.0 with Unique New Features

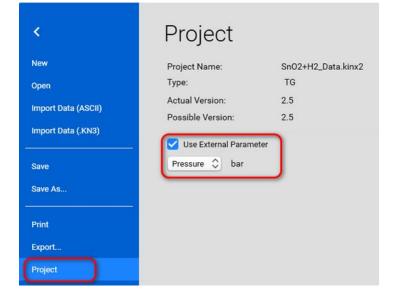
Elena Moukhina 2024





- 1. Reactions depending on additional parameter
- 2. Pressure-dependent reactions
 - 1. Partial Pressure of Gaseous Reactant like Hydrogen for Metal Oxides.
 - 2. Reversible Reactions with Gaseous Reactant in Reverse Reaction
 - 3. Pressure-Dependent Reactions in Inert Gas
- 3. Thermosets, composites, photopolymers:
 - 1. Curing kinetics depending on intensity of UV light
 - 2. Curing reactions with diffusion control (DEA, Rheology)
- 4. Flexible Data Evaluation
 - 1. Evaluation of Arbitrary Data
 - 2. Kinetics for Incomplete Data
 - 3. New Reaction Types
- 5. User Interface (UI) is reworked for native look in Windows 11





Examples of the additional external parameter:

- Partial Pressure of Gaseous Reactant
- Reversible Reactions with Gaseous Reactant in Reverse Reaction
- Pressure-Dependent Reactions in Inert Gas
- Intensity of UV light for curing of photopolymers
- Other parameters

The rate of chemical reactions and crystallization depends on different parameters, the first of them is temperature.

Now we have the possibility to use the second parameter in the common kinetic model, where reaction rate depends on two parameters.



Pressure-Dependent Reactions

2.1 Partial Pressure of Gaseous Reactant2.2 Reversible Reactions with Gaseous Reactant2.3 Pressure-Dependent Reactions in Inert Gas



2.1 Partial Pressure of Gaseous Reactant Reduction of Metal Oxide in H2

total pressure of gas mixture is 1 bar

Reduction of metal from metal oxide in Nitrogen with partial pressure of Hydrogen

Nitrogen with Hydrogen

 $MeO_2 + H_2 \rightarrow Me + H_2O$

$$\frac{d\alpha}{dt} = P_{H2}^{n_p} A \exp\left(\frac{-E_A}{RT}\right) f(\alpha)$$

Hydrogen is the reactive gas.

Reaction rate depends on the hydrogen concentration

the higher partial pressure of hydrogen - the higher reaction rate





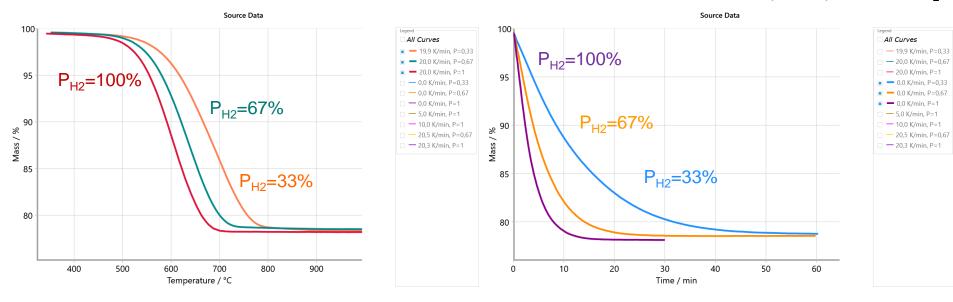
STA 509 with Hydrogen Generator



Data series for analysis

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Isothermal T=600°C, different partial pressure of H₂

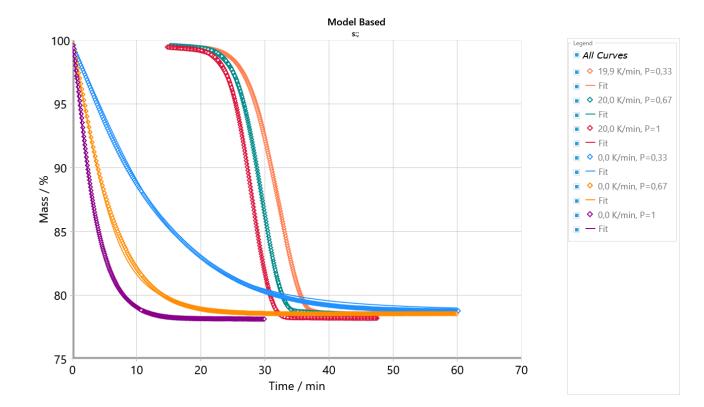


20K/min, different partial pressure of H_2

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Common model in Kinetics Neo depending on the partial pressure of gaseous reactant

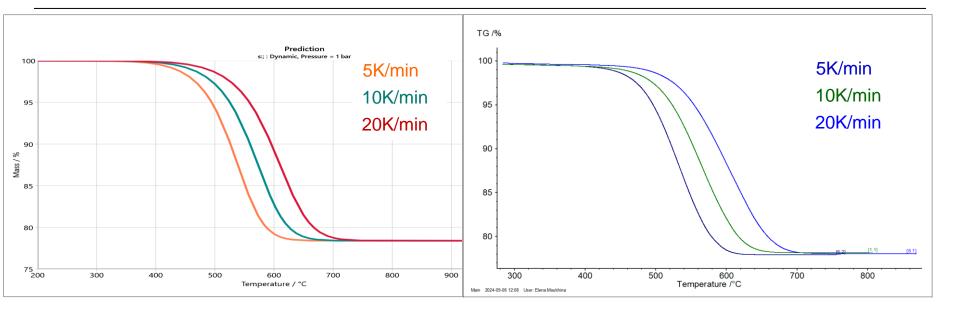




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Verification: Predictions for 100% H₂, different heating rates



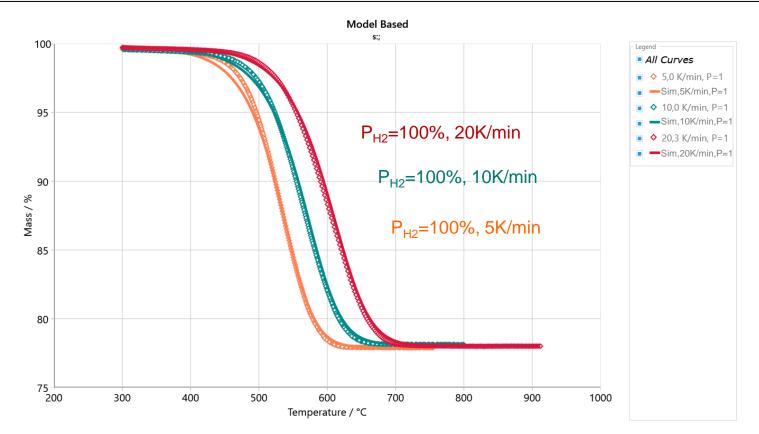


Simulations for 100% of H₂

Experiment

Verification of kinetic model: comparison of simulated and measured data







2.2 Reversible reactions with Gaseous Reactant Decomposition of CaCO₃ under partial pressure of CO₂

total pressure of gas mixture is 1 bar



Reversible reactions

 $A \rightleftharpoons B$

Forward:
$$A \rightarrow B$$
 $A_1 \exp\left(\frac{-E_1}{RT}\right) f_1(\alpha)$ Reverse: $A \leftarrow B$ $A_2 \exp\left(\frac{-E_2}{RT}\right) f_2(\alpha)$

Rection rate total = Reaction rate forward - Reaction rate reverse

$$\frac{d\alpha}{dt} = A_1 \exp\left(\frac{-E_1}{RT}\right) f_1(\alpha) - A_2 \exp\left(\frac{-E_2}{RT}\right) f_2(\alpha)$$

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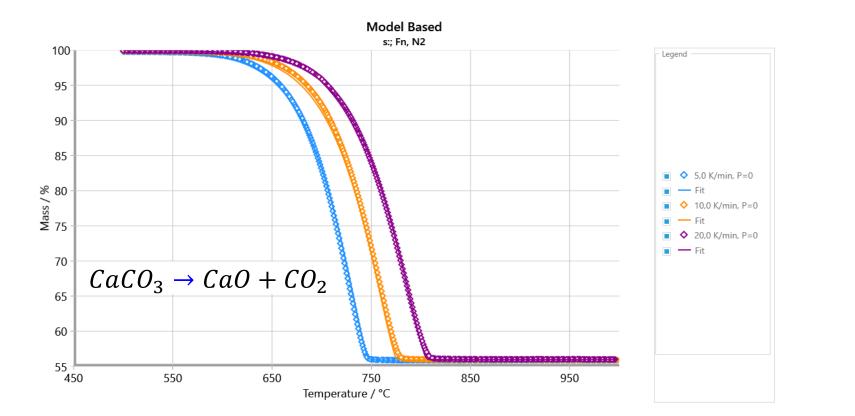


1. Nitrogen only

 $CaCO_3 \rightarrow CaO + CO_2$

$$\frac{d\alpha}{dt} = A \exp\left(\frac{-E_A}{RT}\right) f(\alpha)$$

Decomposition of CaCO₃ in Nitrogen, Pressure=1bar



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1. Nitrogen only (only forward reaction)

$$CaCO_3 \rightarrow CaO + CO_2$$
$$\frac{d\alpha}{dt} = A \exp\left(\frac{-E_A}{RT}\right) f(\alpha)$$

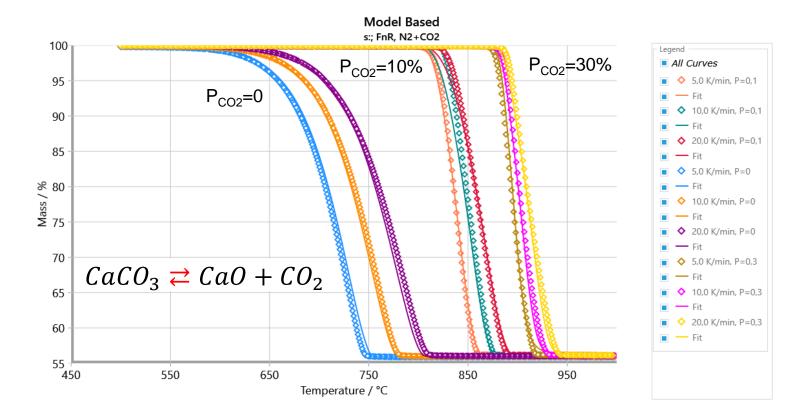
2. Nitrogen with CO_2 (reaction is reversible, P is partial pressure of CO_2)

$$\begin{aligned} CaCO_3 &\rightleftharpoons CaO + CO_2 \\ \frac{d\alpha}{dt} &= A_1 \exp\left(\frac{-E_1}{RT}\right) f_1(\alpha) - P^n A_2 \exp\left(\frac{-E_2}{RT}\right) f_2(\alpha) \end{aligned}$$

 CO_2 is the reactive gas for reverse reaction The rate of reverse reaction depends on the CO_2 concentration The higher partial pressure of CO_2 - the higher rate of reverse reaction and therefore, the total decomposition is later

Common kinetic model for decomposition of $CaCO_3$ in Nitrogen with partial pressure CO_2 (total Pressure=1 bar)





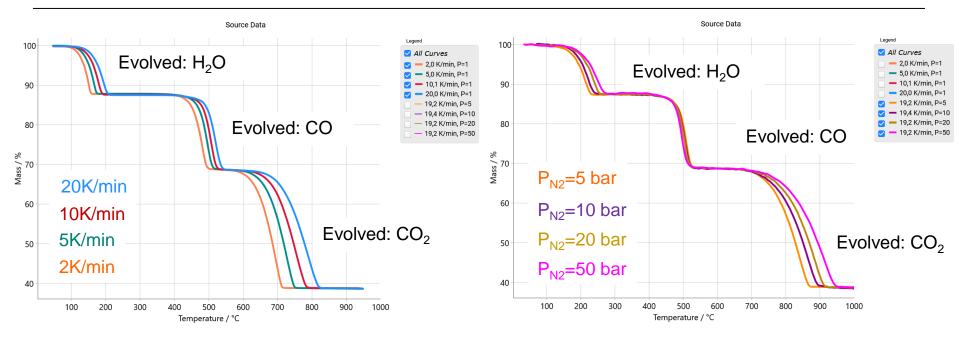


2.3 Pressure-Dependent Reactions in Inert Gas Decomposition of CaOx*H₂O under high pressure of N₂

total pressure of N2 is from 1 to 50 bar

CaOx*H2O at different heating rates and different pressure of N2





normal pressure 1 bar, different heating rates

Heating rate 20K/min, different pressures of N2



Nitrogen, High Pressure

$$CaC_2O_4 * H_2O \rightleftharpoons CaC_2O_4 + H_2O$$
$$CaC_2O_4 \rightarrow CaCO_3 + CO$$
$$CaCO_3 \rightleftharpoons CaO + CO_2$$

 N_2 is the inert gas. It has no influence on the forward reactions for all steps.

It has no influence on the second step, because the second step is non-reversible reaction.

For high pressure of N_2 the diffusion coefficient is lower and the products (H_2O for the first step and CO_2 for the third step) can not be removed fast from reaction zone.

Then for high pressure the reverse reaction is faster, and the total decomposition is later.

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Step 1: reaction is reversible, prefix F: forward reaction, B: reverse reaction, P is pressure of N₂

 $CaC_2O_4 * H_2O \rightleftharpoons CaC_2O_4 + H_2O$

$$\frac{d\alpha}{dt} = A_{1F} \exp\left(\frac{-E_{1F}}{RT}\right) f_{1F}(\alpha) - A_{1B} \exp\left(\frac{-E_{1B}}{RT}\right) f_{1B}(\alpha) \qquad = P^{n1} A_1 \exp\left(\frac{-E_1}{RT}\right) f_1(\alpha)$$

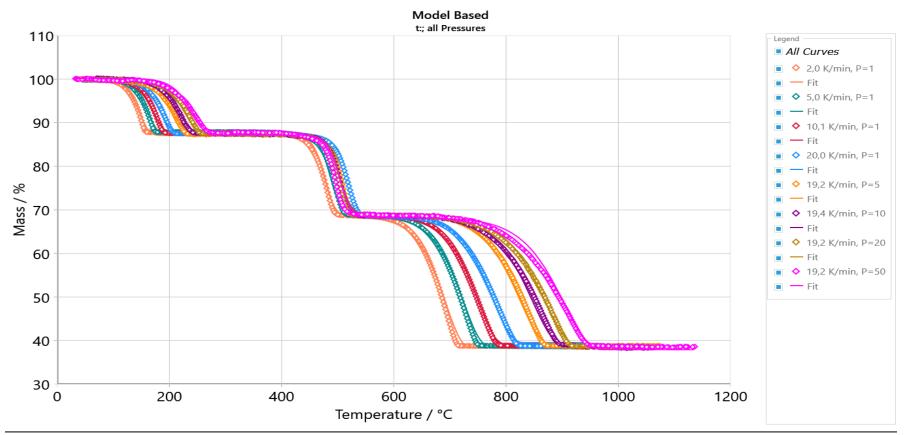
Step 2: only forward reaction

$$CaC_2O_4 \rightarrow CaCO_3 + CO$$
$$\frac{d\alpha}{dt} = A_2 \exp\left(\frac{-E_2}{RT}\right) f_2(\alpha)$$

Step 3: reaction is reversible, prefix F: forward reaction, B: reverse reaction, P is pressure of N₂

$$\begin{aligned} CaCO_3 \rightleftharpoons CaO + CO_2 \\ \frac{d\alpha}{dt} &= A_{3F} \exp\left(\frac{-E_{3F}}{RT}\right) f_{3F}(\alpha) - A_{3B} \exp\left(\frac{-E_{3B}}{RT}\right) f_{3B}(\alpha) \\ &= P^{n3} A_3 \exp\left(\frac{-E_3}{RT}\right) f_3(\alpha) \end{aligned}$$

Common kinetic model for decomposition of $CaC_2O_4^*H_2O_1$ in Nitrogen, different pressures from 1 bar to 50 bar, different heating rates: see legend



Optimal parameters for pressure: $n_1 = -0.75$, $n_3 = -0.73$

NETZSEH





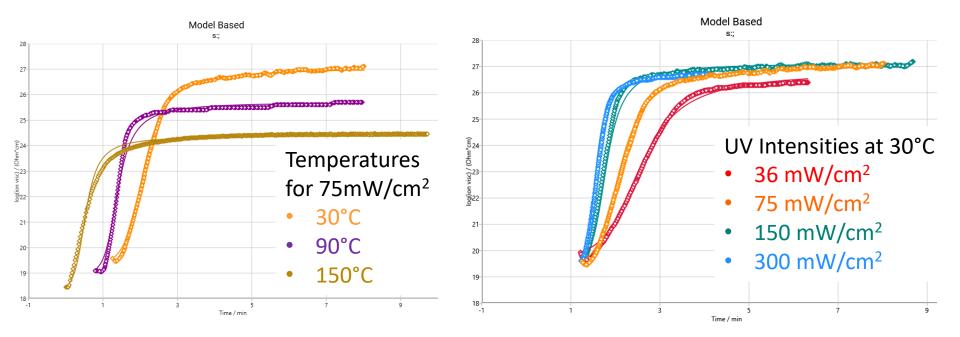
Thermosets, composites, photopolymers 3.1 UV intensity for DSC, DEA 3.2 Diffusion control for DEA, Rheology



3 Curing depending on intensity of UV light

UV curing at different temperatures and different intensities (10kHz)



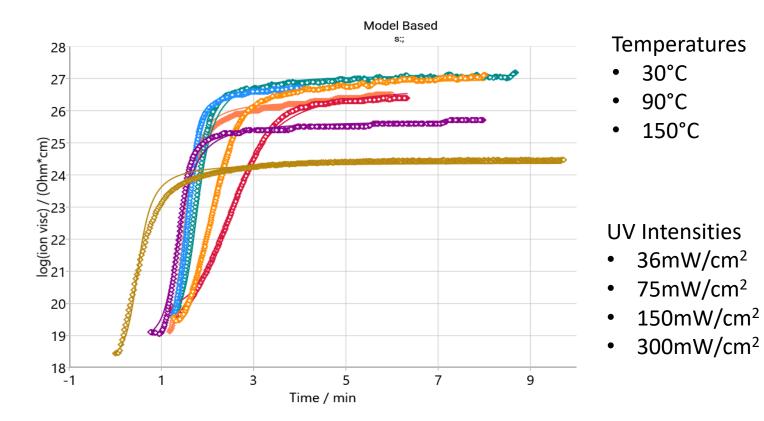


Isothermal DEA measurements at 30°C, 90°C, 150°C for light exposure at 75mW/cm²

Isothermal DEA measurements at 30°C for light exposure at different intensities from 75mW/cm² to 150mW/cm²

Common model in Kinetics Neo depending on both temperature and the intensity of UV light

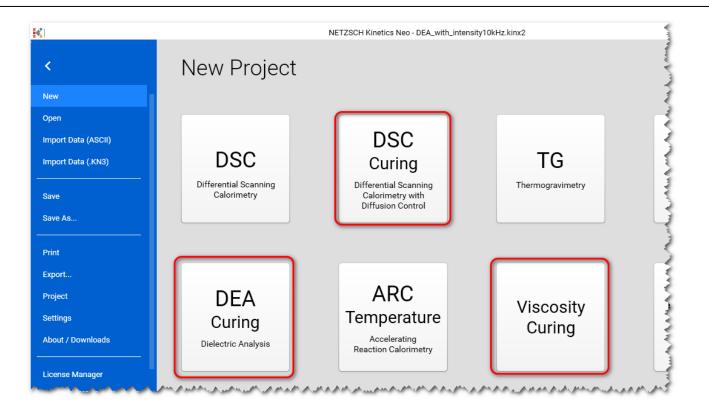






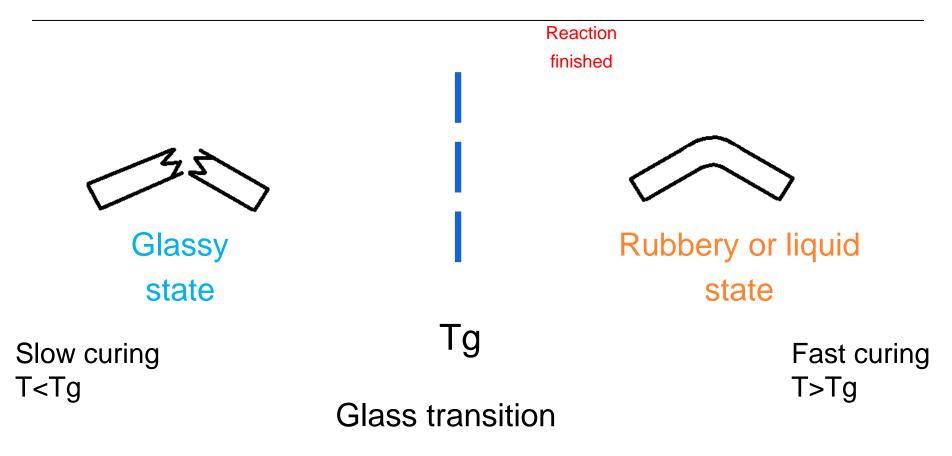
3.2 Diffusion control for DEA, Rheology





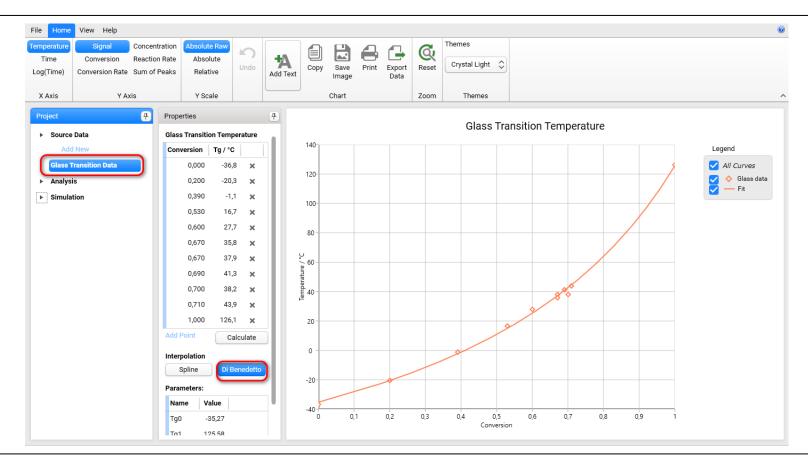
Reactions of curing and cross-linking near glass transition temperature are diffusion controlled





Kinetic analysis of DEA data for curing with diffusion control

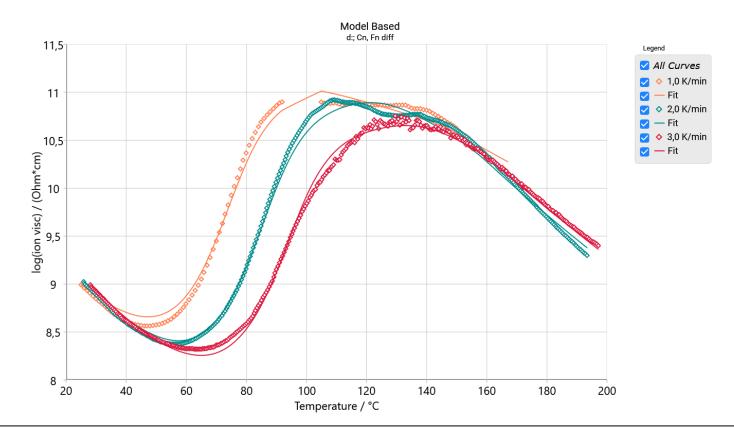




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Kinetics on DEA Data for epoxy curing with diffusion control





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Flexible Data Evaluation

- 4.1 Evaluation of arbitrary data
- 4.2 Kinetics for incomplete data
- 4.3 New reaction types

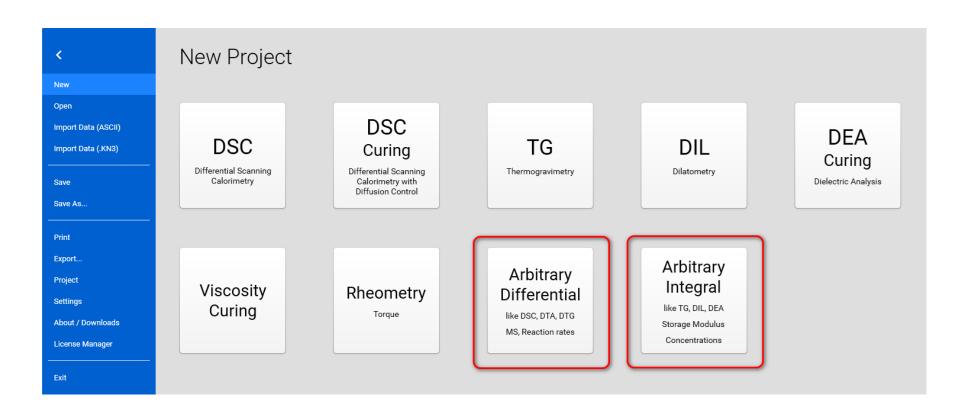


4.1 Evaluation of Arbitrary Data • Differential data

• Integral data

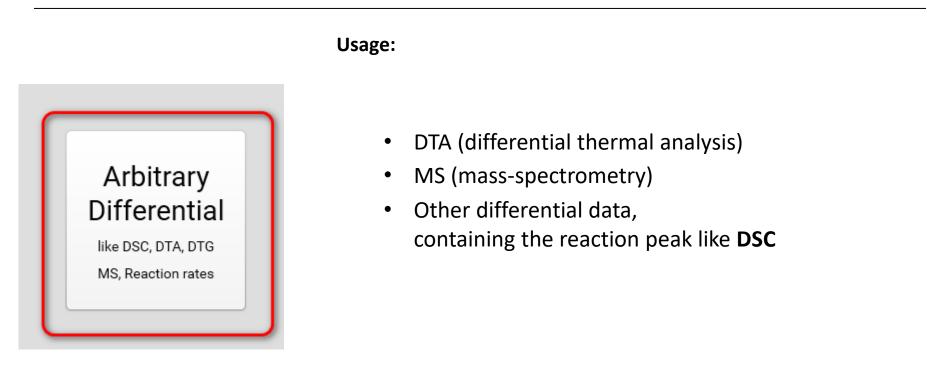
Arbitrary data





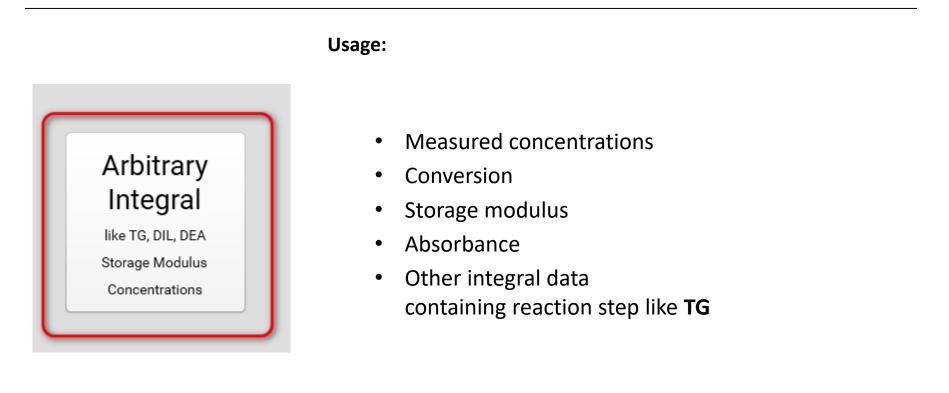
Arbitrary differential data





Arbitrary Integral Data



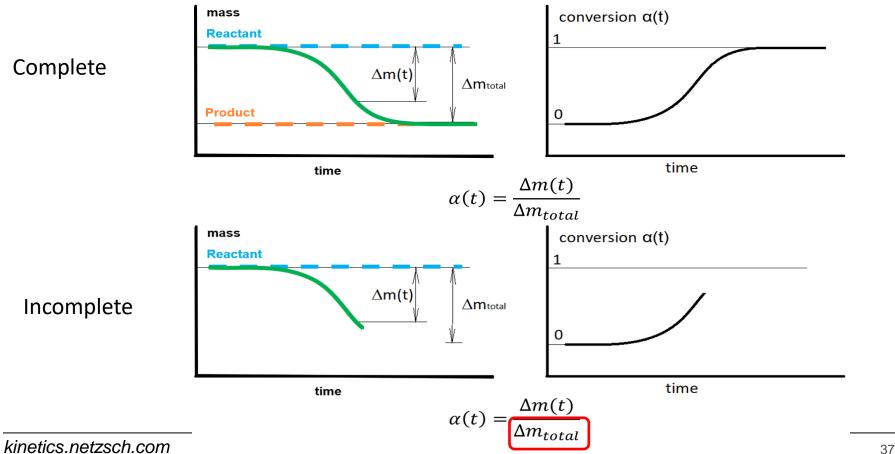




4.2 Kinetics for Incomplete Data

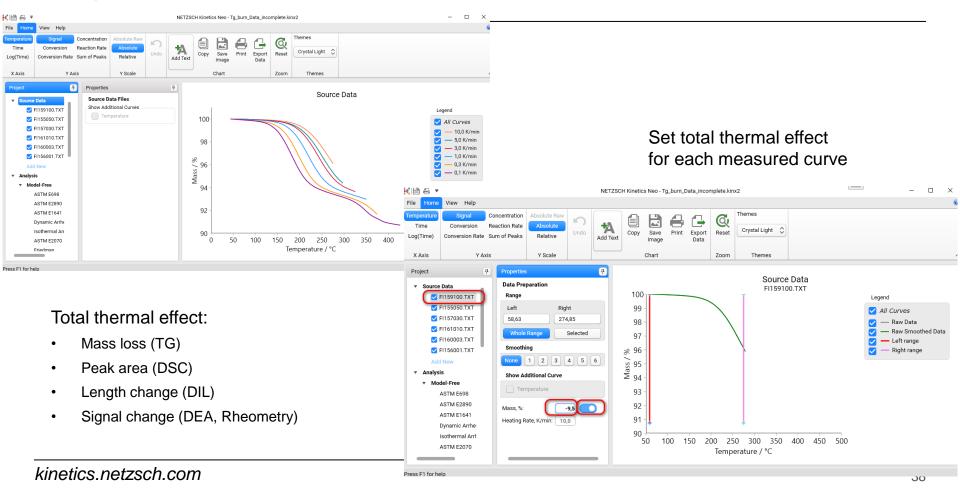
Incomplete Measured Data: Final Part of Reaction Is not Present





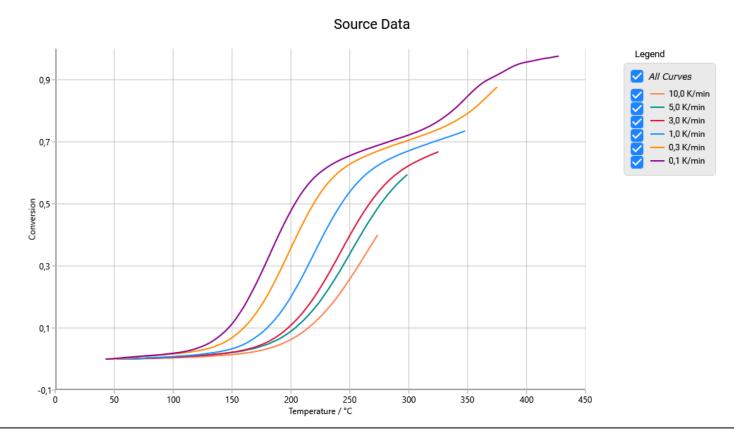
Incomplete Measured Data





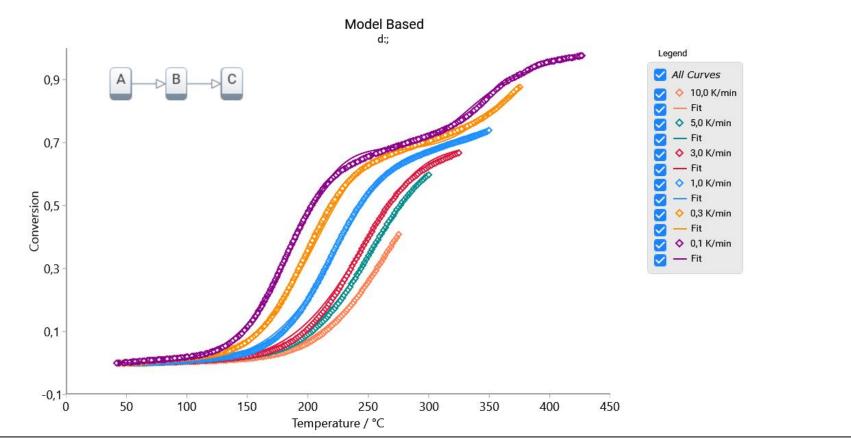
Incomplete Measured Data: Final Part of Reaction Is not Present





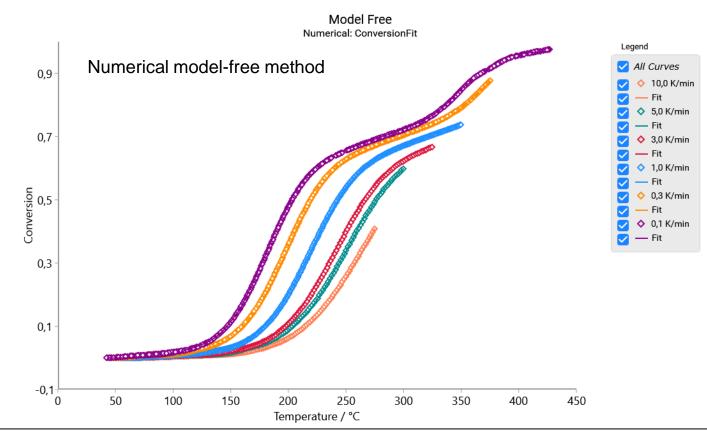
Model Based Analysis for Incomplete Data





NEW: Model-Free Analysis for Incomplete Measured Data







New Reaction Types 4.3

- Reversible reactions ٠
- Reaction of n-th order with diffusion •



NEW: FnR
$$A \rightleftharpoons B$$
Forward: $A \rightarrow B$ $A_1 \exp\left(\frac{-E_1}{RT}\right) f_1(\alpha)$ Reverse: $A \leftarrow B$ $A_2 \exp\left(\frac{-E_2}{RT}\right) f_2(\alpha)$

$$\frac{d\alpha}{dt} = A_1 \exp\left(\frac{-E_1}{RT}\right) f_1(\alpha) - A_2 \exp\left(\frac{-E_2}{RT}\right) f_2(\alpha)$$

Rection rate total = Reaction rate forward – Reaction rate reverse



3-dimensional diffusion in the literature

D3:Jander

 $1.5 * (1-\alpha)^{2/3} / (1-(1-\alpha)^{1/3})$

D4:Ginstling-Brounstein

Zhuravlev-Lasokin-Tempelman

 $1.5 * (1 - \alpha)^{1/3} / (1 - (1 - \alpha)^{1/3})$

 $1.5 * (1 - \alpha)^{5/3} / (1 - (1 - \alpha)^{1/3})$

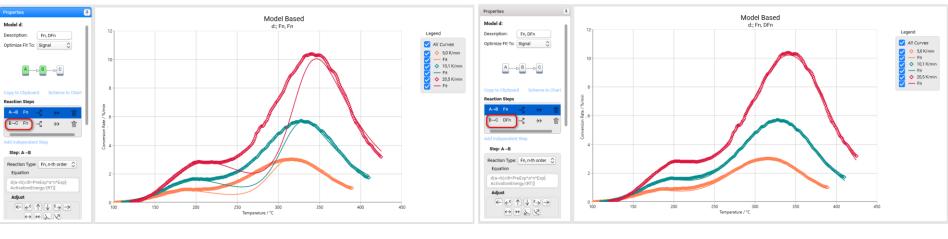
General equation: $1.5 * (1 - \alpha)^n / (1 - (1 - \alpha)^{1/3})$

https://doi.org/10.1016/S0040-6031(03)00222-3

1-dimensional diffusion

D1: 0.5 / a NEW DFn: 0.5 / a * (1- a)ⁿ

Reaction of n-th order with one-dimensional diffusion for decomposition



Fn

NEW: DFn

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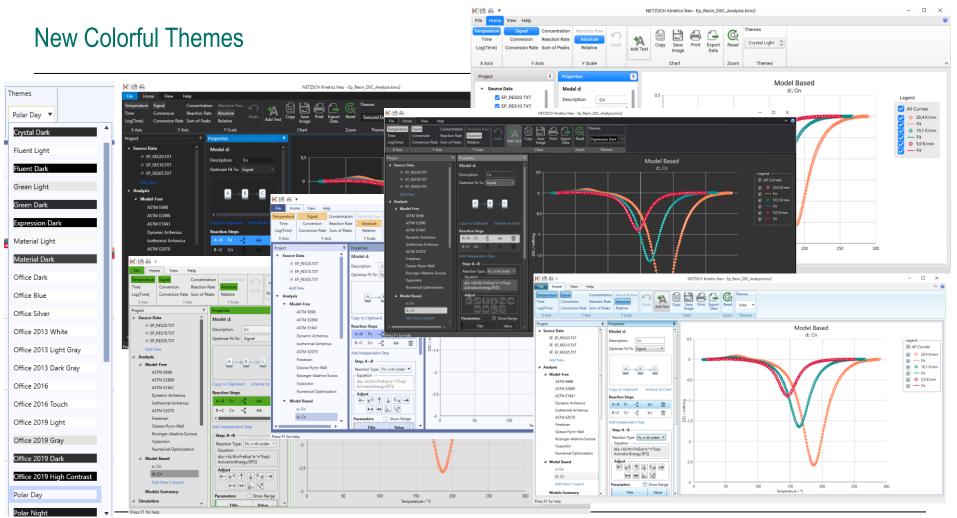
New reaction type **DFn** for the *first-dimensional diffusion with n-th order*. **DFn** reaction type considers diffusion process in the material during decomposition. It adds the diffusion mechanism to the classical reaction of n-th order (Fn).





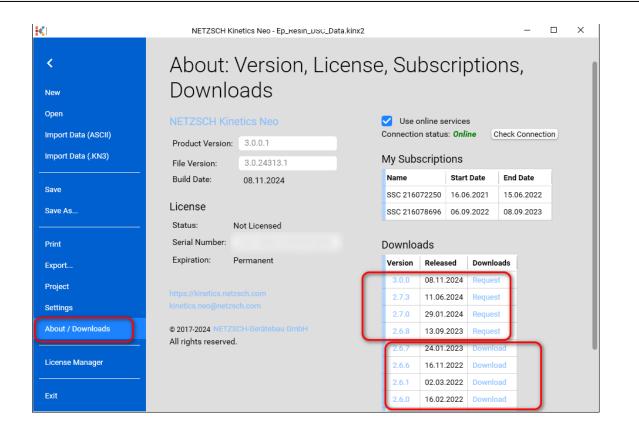
User Interface (UI) is reworked for native look in Windows 11

New colorful themes



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